Contents

Preface xv

1Shale Gas as an Option for the Production of Chemicals and
Challenges for Process Intensification1

Andrea P. Ortiz-Espinoza and Arturo Jiménez-Gutiérrez

- 1.1 Introduction 1
- 1.2 Where Is It Found? 1
- 1.3 Shale Gas Composition *3*
- 1.4 Shale Gas Effect on Natural Gas Prices 3
- 1.5 Alternatives to Produce Chemicals from Shale Gas 4
- 1.6 Synthesis Gas 4
- 1.7 Methanol 5
- 1.8 Ethylene 6
- 1.9 Benzene 7
- 1.10 Propylene 7
- 1.11 Process Intensification Opportunities 8
- 1.12 Potential Benefits and Tradeoffs Associated with Process Intensification *10*
- 1.13 Conclusions 11 References 11
- 2 Design and Techno-Economic Analysis of Separation Units to Handle Feedstock Variability in Shale Gas Treatment 15 Eric Bohac, Debalina Sengupta, and Mahmoud M. El-Halwagi
- 2.1 Introduction 15
- 2.2 Problem Statement 16
- 2.3 Methodology 17
- 2.4 Case Study 17
- 2.4.1 Data 18
- 2.4.2 Process Simulations and Economic Evaluation 19
- 2.4.2.1 Changes in Fixed and Variable Costs 20
- 2.4.2.2 Revenue 21
- 2.4.2.3 Economic Calculations 21
- 2.4.3 Safety Index Calculations 22
- 2.5 Discussion 23

- 2.5.1 Process Simulations 23
- 2.5.1.1 Dehydration Process 23
- 2.5.1.2 NGL Recovery Process 23
- 2.5.1.3 Fractionation Train 26
- 2.5.1.4 Acid Gas Removal 26
- 2.5.2 Profitability Assessment 26
- 2.5.3 High Acid Gas Case Economics 30
- 2.5.4 Safety Index Results 30
- 2.5.5 Sensitivity Analysis 32
- 2.5.5.1 Heating Value Cases 33
- 2.5.5.2 NGL Price Cases 34
- 2.6 Conclusions 35 Appendices 35
 2.A Appendix A: Key Parameters for the Dehydration Process 36
 2.B Appendix B: Key Parameters for the Turboexpander Process 36
 2.C Appendix C: Key Parameters for the Fractionation Train 37
 2.D Appendix D: Key Parameters for the Acid Gas Removal System 37 References 39
- 3 Sustainable Design and Model-Based Optimization of Hybrid RO–PRO Desalination Process 43

Zhibin Lu, Chang He, Bingjian Zhang, Qinglin Chen, and Ming Pan

- 3.1 Introduction 43
- 3.2 Unit Model Description and Hybrid Process Design 47
- 3.2.1 The Process Description 47
- 3.2.2 Unit Model and Performance Metrics 49
- 3.2.2.1 RO Unit Model 49
- 3.2.2.2 PRO Unit Model 52
- 3.2.3 The RO–PRO Hybrid Processes 54
- 3.2.3.1 Open-Loop Configuration 54
- 3.2.3.2 Closed-Loop Configuration 55
- 3.3 Unified Model-Based Analysis and Optimization 56
- 3.3.1 Dimensionless Mathematical Modeling 56
- 3.3.2 Mathematical Model and Objectives 58
- 3.3.3 Optimization Results and Comparative Analysis 59
- 3.4 Conclusion 62 Nomenclature 63 References 65
- 4 Techno-economic and Environmental Assessment of Ultrathin Polysulfone Membranes for Oxygen-Enriched Combustion 69 Serene Sow Mun Lock, Kok Keong Lau, Azmi Mohd Shariff, Yin Fong Yeong, and Norwahyu Jusoh
- 4.1 Introduction 69
- 4.2 Numerical Methodology for Membrane Gas Separation Design 70
- 4.3 Methodology 73

- 4.3.1 Simulation and Elucidation of Mixed Gas Transport Properties of Ultrathin PSF Membranes (Molecular Scale) 73
- 4.3.2 Simulation of Mathematical Model Interfaced in Aspen HYSYS for Mass and Heat Balance (Mesoscale) 75
- 4.3.3 Design of Oxygen-Enriched Combustion Using Ultrathin PSF Membranes 75
- 4.4 Results and Discussion 77
- 4.4.1 Simulation and Elucidation of Mixed Gas Transport Properties of Ultrathin PSF Membranes (Molecular) 77
- 4.4.2 Simulation of Mathematical Model Interfaced in Aspen HYSYS for Mass and Heat Balance (Mesoscale) 79
- 4.4.3 Design of Oxygen-Enriched Combustion Using Ultrathin PSF Membranes 82
- 4.4.3.1 Membrane Area Requirement 82
- 4.4.3.2 Compressor Power Requirement 83
- 4.4.3.3 Turbine Power Requirement 85
- 4.4.3.4 Economic Parameter 88
- 4.5 Conclusion 90 Acknowledgment 91 References 91
- 5 Process Intensification of Membrane-Based Systems for Water, Energy, and Environment Applications 97

Nik A. H. M. Nordin, Zulfan A. Putra, Muhammad R. Bilad, Mohd D. H. Wirzal, Lila Balasubramaniam, Anis S. Ishak, and Sawin Kaur Ranjit Singh

- 5.1 Introduction 97
- 5.2 Membrane Electrocoagulation Flocculation for Dye Removal 99
- 5.3 Carbonation Bioreactor for Microalgae Cultivation *102*
- 5.4 Forward Osmosis and Electrolysis for Energy Storage and Treatment of Emerging Pollutant *107*
- 5.5 Conclusions and Future Perspective *111* References *113*
- 6 Design of Internally Heat-Integrated Distillation Column (HIDiC) 117

Vasu Harvindran and Dominic C. Y. Foo

- 6.1 Introduction *117*
- 6.2 Example and Conceptual Design of Conventional Column *119*
- 6.3 Basic Design of HIDiC *120*
- 6.4 Complete Design of HIDiC 122
- 6.4.1 Top-Integrated Column 122
- 6.4.2 Bottom-Integrated Column 123
- 6.4.3 Geometrical Analysis for Heat Panels 124
- 6.5 Energy Savings and Economic Evaluation 126
- 6.6 Concluding Thoughts 128
 - References 128

x Contents

7	Graphical Analysis and Integration of Heat Exchanger
	Networks with Heat Pumps 131
	Minbo Yang and Xiao Feng
7.1	Introduction 131
7.2	Influences of Heat Pumps on HENs 132
7.2.1	Case 1 133
7.2.2	Case 2 134
7.2.3	Case 3 134
7.2.4	Case 4 135
7.2.5	Case 5 136
7.2.6	Case 6 136
7.2.7	Case 7 136
7.3	Integration of Heat Pump Assisted Distillation in the Overall
	Process 138
7.3.1	Increase of Pinch Temperature 138
7.3.2	Decrease of Pinch Temperature 140
7.3.3	No Change in Pinch Temperature 141
7.3.4	Heat Pump Placement 142
7.4	Case Study 145
7.5	Conclusion 148
	References 148
8	Insightful Analysis and Integration of Reactor and Heat
	Exchanger Network 151
	Di Zhang, Guilian Liu, and Xiao Feng
8.1	Introduction 151
8.2	Influence of Temperature Variation on HEN 152
8.2.1	Location of Cold and Hot Streams 152
8.2.2	Effect of Temperature Variation 153
8.3	Relation Among Reactor Parameters 156
8.3.1	Relation Among Temperatures, Selectivity, and Conversion of
0011	Reactor 157
8.3.1.1	CS1R 159
8.3.1.2	PFR 159
8.3.2	Reactor Characteristic Diagram 160
8.4	Coupling Optimization of HEN and Reactor 161
8.5	Case Study 163
8.6	Conclusions 165
	References 166
9	Fouling Mitigation in Heat Exchanger Network Through
-	Process Ontimization 167
	Yufei Wana and Xiao Fena
91	Introduction 167
9.1	Operation Parameter Optimization for Fouling Mitigation in
1.4	HENs 169
9.2.1	Description on Velocity Optimization 169

- 9.2.2 Fouling Threshold Model 171
- 9.2.3 Heat Transfer Related Models 172
- 9.2.4 Pressure Drop Related Models 174
- 9.3 Optimization of Cleaning Schedule 175
- 9.4 Application of Backup Heat Exchangers 175
- 9.5 Optimization Constraints and Objective Function 176
- 9.5.1 Optimization Constraints 176
- 9.5.2 Objective Function 177
- 9.5.3 Optimization Algorithm 178
- 9.6 Case Studies 178
- 9.6.1 Case Study 1: Consideration of Velocity Optimization Alone 178
- 9.6.1.1 Optimization Results 180
- 9.6.2 Case Study 2: Simultaneous Consideration of Velocity and Cleaning Schedule Optimization *186*
- 9.6.2.1 Constraints for Case Study 188
- 9.6.2.2 Results and Discussion 189
- 9.6.2.3 Considering Backup Heat Exchanger 194
- 9.7 Conclusion 194 Acknowledgments 196 References 198
- 10Decomposition and Implementation of Large-Scale Interplant
Heat Integration201

Runrun Song, Xiao Feng, Mahmoud M. El-Halwagi, and Yufei Wang

- 10.1 Introduction 201
- 10.1.1 Reviews and Discussions for Stream Selection 202
- 10.1.2 Reviews and Discussions for Plant Selection 204
- 10.1.3 Reviews and Discussions for Plant Integration 204
- 10.2 Methodology 205
- 10.2.1 Strategy 1 Overview 205
- 10.2.2 Identification of Heat Sources/Sinks for IPHI from Individual Plants 206
- 10.2.3 Decomposition of a Large-Scale IPHI Problem into Small-Scale Subsections 207
- 10.2.4 Strategy 2 for Indirect IPHI 209
- 10.3 Case Study 212
- 10.3.1 Example 1 212
- 10.3.2 Example 2 215
- 10.4 Conclusion 217 References 218
- 11 Multi-objective Optimisation of Integrated Heat, Mass and Regeneration Networks with Renewables Considering Economics and Environmental Impact 221 So-Mang Kim, Adeniyi J. Isafiade, and Michael Short
- 11.1 Introduction 221
- 11.2 Literature Review 222

- 11.2.1 Regeneration in Process Synthesis 222
- 11.2.2 The Analogy of MEN and REN 222
- 11.2.3 Combined Heat and Mass Exchange Networks (CHAMENs) 224
- 11.3 Environmental Impact in Process Synthesis 225
- 11.3.1 Life Cycle Assessment 225
- 11.4 The Synthesis Method and Model Formulation 226
- 11.4.1 Synthesis Approach 227
- 11.4.2 Assumptions 229
- 11.4.3 MINLP Model Formulation 230
- 11.4.3.1 HENS Model Equations 230
- 11.4.3.2 MEN and REN Model Equations 233
- 11.4.3.3 The Combined Economic Objective Function 236
- 11.4.3.4 Initializations and Convergence 239
- 11.5 Case Study 240
- 11.5.1 H₂S Removal 240
- 11.5.1.1 Synthesis of MEN (The First Step) 242
- 11.5.1.2 Simultaneous Synthesis of MEN and REN (The Second Step) 243
- 11.5.1.3 Simultaneous Synthesis of MEN, REN, and HEN (The Third Step) 244
- 11.5.1.4 Absorption and Regeneration Temperature Optimization 247
- 11.5.1.5 The Synthesis of Combined Model Using MOO 252
- 11.6 Conclusions and Future Works 254 References 256
- 12 Optimization of Integrated Water and Multi-regenerator Membrane Systems Involving Multi-contaminants: A Water-Energy Nexus Aspect 261 Musah Abass and Thokozani Maiozi
- 12.1 Introduction 261
- 12.2 Problem Statement 263
- 12.3 Model Formulation 263
- 12.3.1 Material Balances for Sources 264
- 12.3.2 Mass and Contaminants Balances for Regeneration Units 265
- 12.3.3 Mass and Contaminant Balances for Permeate and Reject Streams 265
- 12.3.4 Mass and Contaminant Balances for Sinks 266
- 12.3.5 Modeling of the Regeneration Units 266
- 12.3.5.1 Performance of Regeneration Units 266
- 12.3.6 Logical Constraints 267
- 12.3.7 The Objective Function 267
- 12.4 Illustrative Example 268
- 12.5 Conclusion 272
 12.5 Conclusion 272
 12.A Appendix: Detailed Models for the ED and RO Modules 273
 Nomenclature 280
 References 282

- 13 Optimization Strategies for Integrating and Intensifying Housing Complexes 285
 - Jesús M. Núñez-López, and José M. Ponce-Ortega
- 13.1 Introduction 285
- 13.2 Methods 288
- 13.2.1 Total Annual Cost for the Integrated System 289
- 13.2.2 Fresh Water Consumption 289
- 13.2.3 GHGE Emissions 290
- 13.2.4 Environmental Impact 290
- 13.2.5 Sustainability Return of Investment 293
- 13.2.6 Process Route Healthiness Index 293
- 13.2.7 Multistakeholder Approach 295
- 13.3 Case Study 295
- 13.4 Results 296
- 13.5 Conclusions 296 References 299

14 Sustainable Biomass Conversion Process Assessment 301 Eric C. D. Tan

- 14.1 Introduction 301
- 14.2 Methodology and Assumptions 302
- 14.3 Results and Discussion 305
- 14.3.1 Environmental Indicators 305
- 14.3.2 Energy Indicators 310
- 14.3.3 Efficiency Indicators 312
- 14.3.4 Economic Indicators 313
- 14.4 Conclusions 314
 - Acknowledgments 316
 - References 317

Index 319